

ROLL NO : MS [] [] [] [] NAME :

PHY202 Jan-Aug 2020: Midsem 1 Dated February 4, 2020: Inst: Dipanjan Chakraborty

- Time : 60 minutes
- Max Marks : 40
- Attempt all questions. No aids (Books/Notes/Gadgets).

Question	1	2	3	4	T
Marks					

1. Each of the following question has 1 marks for the correct tick mark and the rest for justification.

(a): The differential $dz = (2xy^3 + 2)dx + (3x^2y^2 + e^y)dy$, is not an exact differential.

[4]
YES NO

Justification

$$dz = A(x,y) dx + B(x,y) dy$$

$$\frac{\partial A}{\partial y} = 6xy^2 \quad \text{--- (1)}$$

$$\frac{\partial B}{\partial x} = 6xy^2 \quad \text{--- (1)}$$

$$\frac{\partial A}{\partial y} = \frac{\partial B}{\partial x} \quad \text{--- (1)}$$

Hence Exact differential.

$$\frac{\partial z}{\partial x} = 2xy^3 + 2$$

$$z = 2 \cdot \frac{x^2}{2} y^3 + 2x + f(y) \quad \text{--- (1)}$$

$$\frac{\partial z}{\partial y} = 3x^2 y^2 + e^y$$

$$z = x^2 y^3 + e^y + g(x) \quad \text{--- (1)}$$

By comparison

$$z = x^2 y^3 + 2x + e^y \quad \text{--- (1)}$$

Hence exact.

Possibility to show that $\int_C dz = 0$.
by choosing appropriate path.

(b): In an adiabatic process, the work done from taking a system from a volume V_1 to V_2 is more for n moles a diatomic gas than for n moles of monoatomic gas.

[1] YES NO

Justification

$$W = p dV = \alpha \int \frac{dV}{V^r} = \alpha \left. \frac{V^{-r+1}}{-r+1} \right|_{V_1}^{V_2} \quad \text{--- (1)}$$

$$= \alpha \frac{V_2^{(1-r)} - V_1^{(1-r)}}{(1-r)} = \frac{P_2 V_2 - P_1 V_1}{(1-r)} \quad \text{--- (1)}$$

$$P_1 V_1^r = \alpha$$

$$P_2 V_2^r = \alpha$$

r for monoatomic is $5/3$
 r for diatomic is $7/5$

$\therefore W = \frac{3}{2} (P_1 V_1 - P_2 V_2)$ ~~mono~~-monoatomic --- (1)

$W = \frac{5}{2} (P_1 V_1 - P_2 V_2)$ Diatomic.

(c): An ideal monoatomic gas, at a temperature T_0 is mixed with an equal volume of an ideal diatomic gas at a temperature $2T_0$. The final temperature of the mixture is $13T_0/8$. [4]

YES NO

Justification

Both are possible answers.
If the work done is zero
then heat given up is taken by other.
Assuming constant volume

$$C_1(T_f - T_1) = C_2(T_2 - T_f) \quad \text{--- (1)}$$

$$T_f = \frac{C_1 T_1 + C_2 T_2}{C_1 + C_2} \quad \text{--- (2)}$$

$$C_1 = 3/2; \quad T_1 = T_0$$

$$C_2 = 5/2; \quad T_2 = 2T_0 \quad T_f = \frac{13T_0}{8} \quad \text{--- (1)}$$

There are other possibilities.
For example $\Delta S = \Delta S_1 + \Delta S_2 = 0$.

(3)

(d): Given the fundamental equation for a thermodynamic system as $S = A(nVU)^{1/3}$, the equation of state is $P/T = (A/3)\sqrt{A/3}\sqrt{nT/V}$. [4]

YES NO

Justification

$$S = A(nVU)^{1/3} \quad \left. \begin{aligned} \left. \frac{\partial S}{\partial V} \right)_{U, n} = \frac{P}{T} = \frac{1}{3} A n^{1/3} U^{1/3} V^{-2/3} \right\} \text{--- (1)} \end{aligned}$$

$$\left. \begin{aligned} \left. \frac{\partial S}{\partial U} \right)_{n, V} = A V^{1/3} n^{1/3} \left(\frac{1}{3}\right) U^{-2/3} = \frac{1}{T} \right\} \end{aligned}$$

$$\Rightarrow \frac{A}{3} \frac{V^{1/3} n^{1/3}}{U^{2/3}} = \frac{1}{T}$$

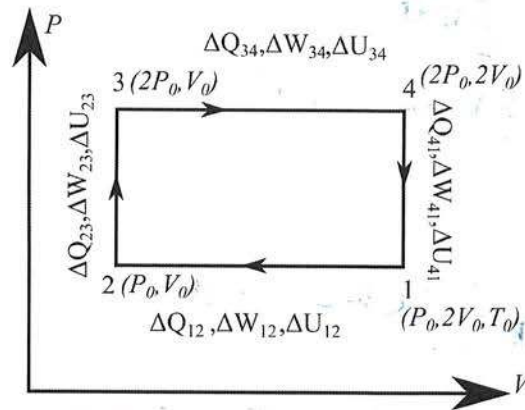
$$U^2 = \left(\frac{A}{3}\right)^3 V n T^3$$

$$U = \left(\frac{A}{3}\right)^{3/2} V^{1/2} n^{1/2} T^{3/2}$$

$$\frac{P}{T} = \left(\frac{A}{3}\right) \frac{n^{1/3}}{V^{2/3}} V^{1/6} n^{1/6} T^{1/2} \left(\frac{A}{3}\right)^{1/2} \quad U^{1/3} = \left(\frac{A}{3}\right)^{1/2} V^{1/6} n^{1/6} T^{1/2} \quad \text{--- (1)}$$

$$= \left(\frac{A}{3}\right)^{3/2} \frac{n^{1/2} T^{1/2}}{V^{1/2}} = \frac{A}{3} \sqrt{\frac{A}{3}} \sqrt{\frac{nT}{V}} \quad \text{--- (1)}$$

2. Consider a system of ideal monoatomic gas that is taken through the cycle shown in the figure. The numerals and the corresponding arrows represents the direction of the thermodynamic processes. The corresponding values of pressure and volume are also indicated in the diagram. All processes are considered to be reversible. Let ΔQ_{ij} , ΔU_{ij} , ΔW_{ij} represent the change in heat (taken/or given up), the change in internal energy and the work done between the consecutive points i and j in the diagram. [Marks=6+6]



(a): Calculate the quantities ΔQ_{ij} , ΔU_{ij} , ΔW_{ij} between the consecutive points i and j as shown in the diagram. From this calculate the total heat change in the cyclic process.

$$\Delta W_{12} = -P_0 \int_{V_1}^{V_2} dV = -P_0(V_0 - 2V_0) = P_0 V_0 = RT_0/2 \quad \frac{2P_0 V_0 = RT_0}{*1}$$

$$\Delta U_{12} = \frac{3}{2} R (T_2 - T_1) = -\frac{3}{4} RT_0$$

$$P_0 V_0 = RT_2 \Rightarrow T_2 = T_0/2 \quad *1$$

①

$$\Delta Q_{12} = \Delta U_{12} - \Delta W_{12} = -\frac{3}{4} RT_0 - \frac{RT_0}{2} = -\frac{5}{4} RT_0$$

$$\Delta W_{23} = 0 \quad \Delta U_{23} = \frac{3}{2} R (T_3 - T_2)$$

$$2P_0 V_0 = RT_3$$

$$\Delta Q_{23} = \frac{3}{2} R (T_0 - T_0/2) = \frac{3}{4} RT_0$$

$$T_3 = T_0 \quad *2$$

①

$$\Delta W_{34} = -2P_0 (V_4 - V_3) = -2P_0 V_0 = -RT_0$$

$$\Delta U_{34} = \frac{3}{2} R (T_4 - T_3)$$

$$4P_0 V_0 = RT_4$$

$$= \frac{3}{2} RT_0$$

$$T_4 = 2T_0 \quad *3$$

①

$$\Delta Q_{34} = \Delta U_{34} - \Delta W_{34} = \frac{3}{2} RT_0 + RT_0 = \frac{5}{2} RT_0$$

$$*1 + *2 + *3 = ①$$

$$\Delta W_{41} = 0 \quad \Delta U_{41} = \frac{3}{2} R (T_1 - T_4) = \frac{3}{2} R (T_0 - 2T_0) = -\frac{3}{2} RT_0 \quad ①$$

$$\Delta Q_{41} = -\frac{3}{2} RT_0$$

$$\Delta Q = \Delta Q_{12} + \Delta Q_{23} + \Delta Q_{34} + \Delta Q_{41} = \frac{RT_0}{2} \quad ①$$

(b): Now calculate the change in the entropy explicitly from the definition $dS = dQ/T$. Is there a contradiction with the result for the heat change for the whole cycle that you obtained earlier?

$$T dS = dU + PdV = \frac{3}{2} R dT + PdV. \quad PV = RT \quad PdV = R dT \quad \text{--- (1)}$$

$$T dS_{12} = \frac{3}{2} R dT + R dT = \frac{5}{2} R dT$$

$$\Delta S_{12} = \frac{5}{2} R \ln T_2/T_1 = -\frac{5}{2} R \ln 2 \quad \text{--- (1)}$$

$$T dS_{23} = dU_{23} = \frac{3}{2} R dT$$

$$\Delta S_{23} = \frac{3}{2} R \ln T_3/T_2 = \frac{3}{2} R \ln 2 \quad \text{--- (1)}$$

$$T dS_{34} = \frac{5}{2} R dT \Rightarrow \Delta S_{34} = \frac{5}{2} R \ln \frac{T_4}{T_3} = \frac{5}{2} R \ln 2. \quad \text{--- (1)}$$

$$T dS_{41} = \frac{3}{2} R dT \quad \Delta S_{41} = \frac{3}{2} R \ln \frac{T_1}{T_4} = -\frac{3}{2} R \ln 2 \quad \text{--- (1)}$$

$$\text{Total change in entropy } \Delta S = 0. \quad \text{--- (1)}$$

3. Consider a thermodynamic system described by the macroscopic variable S, U, V, N , where the symbols have their usual meaning. The equation of states are $U = 3Nk_B T$ and $PV = Nk_B T$. [Marks=4+4+4]

(a): Determine the dependence of the chemical potential μ as a function U, V, N .

Gibbs Duhem relation

$$U d(1/T) + V d(P/T) = N d(\mu/T)$$

$$U d\left(\frac{3Nk_B}{U}\right) + V d\left(\frac{Nk_B}{V}\right) = N d(\mu/T). \quad \text{--- (1)}$$

$$U \left[3Nk_B \left(\frac{dU}{U^2} \right) + \frac{3k_B dN}{U} \right] + V \left[Nk_B \left(\frac{-dV}{V^2} \right) + \frac{k_B dN}{V} \right] = N d(\mu/T)$$

$$-3Nk_B \frac{dU}{U} + 4k_B dN + Nk_B \frac{dV}{V} = N d(\mu/T) \quad \text{--- (1)}$$

$$-3 \frac{dU}{U} + 4 \frac{dN}{N} + \frac{dV}{V} = d(\mu/k_B T) \quad \text{--- (1)}$$

$$\frac{\mu}{k_B T} = \ln \kappa \frac{N^4}{V U^3}$$

where κ is a constant of integration.

$$\hookrightarrow \text{(1)}$$

(b): Now suppose I want the chemical potential μ to be zero, for all values of U, V . Determine N as function of U and V so that $\mu = 0$. Hence determine U and S as a function of T and V .

If $\mu = 0$, then $\frac{k N^4}{V U^3} = 1 \quad N^4 = k V U^3 \Rightarrow N = k V^{1/4} U^{3/4} \quad \text{--- (1)}$

Since $U = 3 N k_B T \Rightarrow U = 3 k V^{1/4} U^{3/4} k_B T$
 $\Rightarrow U^{1/4} = 3 k k_B V^{1/4} T$
 $\Rightarrow \boxed{U = A V T^4} \quad \text{--- (1)}$ $\frac{PV}{T} = 3 N k_B T = k V^{1/4} U^{3/4}$

$S = \frac{U}{T} + \frac{PV}{T} - \frac{\mu N}{T} = \frac{U}{T} + \frac{PV}{T} = 3 N k_B + N k_B = 4 N k_B \quad \text{--- (1)}$
 $N k_B = k k_B V^{1/4} (A V T^4)^{3/4} = k k_B V^{1/4} A^{3/4} V^{3/4} T^3$
 $= \frac{1}{3} A^{1/4} V^{1/4} A^{3/4} V^{3/4} T^3$
 $= \frac{A}{3} V T^3$

$\therefore \boxed{S = \frac{4 A V T^3}{3} = \frac{4}{3} \frac{U}{T}} \quad \text{--- (1)}$

(c): What would be the change in entropy of such a system (that is with $\mu = 0$) if the system is isothermally expanded. Verify that your answer is correct from the expression of S you obtained before.

Isothermal expansion $\rightarrow T$ is constant.

$\therefore \Delta S = \frac{4}{3} A \Delta V T^3 \quad \text{--- (1)}$

~~$dW = P dV = \dots = N k_B T \frac{dV}{V} = N k_B T \ln \frac{V_2}{V_1}$~~

~~$dU = 3 N k_B dT$~~ $\Delta U = A \Delta V T^4$

$\frac{PV}{T} = N k_B = \frac{1}{3} A V T^3 \Rightarrow P = \frac{1}{3} A T^4 \quad \text{--- (1)}$

$\Delta W = -P \int dV = -\frac{1}{3} A T^4 \Delta V \Rightarrow \left. \begin{aligned} dW &= -\frac{1}{3} A T^4 dV \\ dU &= A T^4 dV \end{aligned} \right\} \text{--- (1)}$

$\Delta U = A \Delta V T^4$

$\therefore dQ = dU + dW = \frac{4}{3} A T^4 dV$

$dS = \frac{dQ}{T} = \frac{4}{3} A T^3 dV \Rightarrow \boxed{\Delta S = \frac{4}{3} A T^3 \Delta V} \quad \text{--- (1)}$

Rough Work

[Faint handwritten notes and mathematical derivations, including terms like T, A, and various subscripts, are visible but illegible due to low contrast.]