CHM202

Energetics and dynamics of chemical reactions

Solutions Assignment –IX

Q.1 Set up the rate equations for the reaction mechanism:

$$A \underbrace{\overset{k_a, \ k'_a}{\longleftarrow}} B \underbrace{\overset{k_b, \ k'_b}{\longleftarrow}} C$$

Show that the mechanism is equivalent to

$$A \underset{\frown}{\underbrace{k_{\text{eff}}, k'_{\text{eff}}}} C$$

under specified circumstances.

Sol.:

The rate equations are

$$\frac{d[A]}{dt} = -k_a[A] + k'_a[B]$$

$$\frac{d[B]}{dt} = k_a[A] - k'_a[B] - k_b[B] + k'_b[C]$$

$$\frac{d[C]}{dt} = k_b[B] - k'_b[C]$$

These equations are a set of coupled differential equations and, though it is not immediately apparent, they do admit of an analytical general solution. However, we are looking for specific circumstances under which the mechanism reduces to the second form given. Since the reaction involves an intermediate, let us explore the result of applying the steady-state approximation to it. Then

$$\frac{d[B]}{dt} = k_a[A] - k'_a[B] - k_b[B] + k'_b[C] = 0$$

and [B] =
$$\frac{k_a[A] + k'_b[C]}{k'_a + k_b}$$

Therefore,
$$\frac{d[A]}{dt} = -\frac{k_a k_b}{k'_a + k_b}[A] + \frac{k'_a k'_b}{k'_a + k_b}[C]$$

This rate expression may be compared to that given in the text [Section 22.4] for the mechanism

$$A \underset{k'}{\stackrel{k}{\leftrightarrow}} B \quad \left[\text{here } A \underset{k'_{\text{eff}}}{\stackrel{k_{\text{eff}}}{\leftrightarrow}} C \right]$$

Hence, $k_{\text{eff}} = \frac{k_a k_b}{k'_a + k_b}$ $k'_{\text{eff}} = \frac{k'_a k'_b}{k'_a + k_b}$ The solutions are [A] = $\left(\frac{k'_{\text{eff}} + k_{\text{eff}} e^{-(k'_{\text{eff}} + k_{\text{eff}})t}}{k'_{\text{eff}} + k_{\text{eff}}}\right) \times [A]_0$ [22.23] and [C] = [A]_0 - [A]

Thus, the conditions under which the first mechanism given reduces to the second are the conditions under which the steady-state approximation holds, namely, when B can be treated as a steady-state intermediate. **Q.2** Derive an equation for the steady-state rate of the sequence of reactions $A \rightleftharpoons B \rightleftharpoons C \rightleftharpoons D$, with

[A] maintained at a fixed value and the product D removed as soon as it is formed.

Sol.:

Let the forward rates be written as

$$r_1 = k_1[A], \quad r_2 = k_2[B], \quad r_3 = k_3[C]$$

and the reverse rates as

$$r'_1 = k'_1[B], \quad r'_2 = k'_2[C], \quad r'_3 = k'_3[D]$$

The net rates are then

$$R_1 = k_1[A] - k'_1[B], \quad R_2 = k_2[B] - k'_2[C], \quad R_3 = k_3[C] - k'_3[D]$$

But $[A] = [A]_0$ and [D] = 0, so that the steady-state equations for the net rates of the individual steps are

$$k_1[A]_0 - k'_1[B] = k_2[B] - k'_2[C] = k_3[C]$$

From the second of these equations we find

$$[C] = \frac{k_2[B]}{k_2' + k_3}$$

After inserting this expression for [C] into the first of the steady-state equations we obtain

$$[B] = \frac{k_1[A]_0 + k_2'[C]}{k_1' + k_2} = \frac{k_1[A]_0 + k_2'((k_2[B])/(k_2' + k_3))}{k_1' + k_2}$$

which yields, upon isolating [B],

[B] = [A]₀ ×
$$\frac{k_1}{k'_1 + k_2 - (k_2k'_2/(k'_2 + k_3))}$$

Thus, at the steady state

$$R_1 = R_2 = R_3 = [A]_0 k_1 \times \left(1 - \frac{k_1}{k_1' + k_2 - \left(\frac{k_2 k_2'}{k_2' + k_3}\right)} \right) = \left[\frac{k_1 k_2 k_3 [A]_0}{k_1' k_2' + k_1' k_3 + k_2 k_3} \right]$$

COMMENT. At steady state, not only are the net rates of reactions 1, 2, and 3 steady, but so are the concentrations [B] and [C]. That is,

$$\frac{d[B]}{dt} = k_1[A]_0 - (k'_1 + k_2)[B] + k'_2[C] \approx 0$$

and
$$\frac{d[C]}{dt} = k_2[B] - (k'_2 + k_3)[C] \approx 0$$

In fact, another approach to solving the problem is to solve these equations for [B] and [C].

Q.3 On the basis of the following proposed mechanism, account for the experimental fact that the rate law for the decomposition

$$2N_2O_5(g) \to 4 \text{ NO}_2(g) + O_2(g) \text{ is } v = k[N_2O_5].$$
(1) $N_2O_5 \rightleftharpoons NO_2 + NO_3$ k_1, k'_1
(2) $NO_2 + NO_3 \to NO_2 + O_2 + NO$ k_2
(3) $NO + N_2O_5 \to NO_2 + NO_2 + NO_2$ k_3

Sol.:

The intermediates are NO and NO₃ and we apply the steady-state approximation to each of their concentrations

$$k_{2} [NO_{2}] [NO_{3}] - k_{3} [NO] [N_{2}O_{5}] = 0$$

$$k_{1} [N_{2}O_{5}] - k'_{1} [NO_{2}] [NO_{3}] - k_{2} [NO_{2}] [NO_{3}] = 0$$

Rate = $-\frac{1}{2} \frac{d [N_{2}O_{5}]}{dt}$
 $\frac{d [N_{2}O_{5}]}{dt} = -k_{1} [N_{2}O_{5}] + k'_{1} [NO_{2}] [NO_{3}] - k_{3} [NO] [N_{2}O_{5}]$

From the steady-state equations

$$k_3 [NO] [N_2O_5] = k_2 [NO_2] [NO_3]$$

 $[NO_2] [NO_3] = \frac{k_1 [N_2O_5]}{k'_1 + k_2}$

Substituting,

$$\frac{d[N_2O_5]}{dt} = -k_1[N_2O_5] + \frac{k_1'k_1}{k_1' + k_2}[N_2O_5] - \frac{k_2k_1}{k_1' + k_2}[N_2O_5] = -\frac{2k_1k_2}{k_1' + k_2}[N_2O_5]$$

Rate = $\frac{k_1k_2}{k_1' + k_2}[N_2O_5] = k[N_2O_5]$

Q.4 Consider the acid-catalysed reaction

(1)
$$HA + H^+ \rightleftharpoons HAH^+$$

(2) $HAH^+ + B \rightarrow BH^+ + AH$ k_2 , slow

Deduce the rate law and show that it can be made independent of the specific term [H⁺]. **Sol.**:

The rate of production of the product is

$$\frac{\mathrm{d}\left[\mathrm{B}\mathrm{H}^{+}\right]}{\mathrm{d}t} = k_{2}\left[\mathrm{H}\mathrm{A}\mathrm{H}^{+}\right]\left[\mathrm{B}\right]$$

HAH+ is an intermediate involved in a rapid pre-equilibrium

$$\frac{\left[\mathrm{HAH}^{+}\right]}{\left[\mathrm{HA}\right]\left[\mathrm{H}^{+}\right]} = \frac{k_{1}}{k_{1}'} \operatorname{so}\left[\mathrm{HAH}^{+}\right] = \frac{k_{1} \left[\mathrm{HA}\right]\left[\mathrm{H}^{+}\right]}{k_{1}'}$$

and
$$\frac{\mathrm{d}\left[\mathrm{BH}^{+}\right]}{\mathrm{d}t} = \boxed{\frac{k_{1}k_{2}}{k_{1}'}} \left[\mathrm{HA}\right]\left[\mathrm{H}^{+}\right]\left[\mathrm{B}\right]}$$

This rate law can be made independent of $[H^+]$ if the source of H^+ is the acid HA, for then H^+ is given by another equilibrium

$$\frac{[\mathrm{H}^+][\mathrm{A}^-]}{[\mathrm{HA}]} = K_\mathrm{a} = \frac{[\mathrm{H}^+]^2}{[\mathrm{HA}]} \text{ so } [\mathrm{H}^+] = (K_\mathrm{a}[\mathrm{HA}])^{1/2}$$

and $\frac{\mathrm{d}[\mathrm{B}\mathrm{H}^+]}{\mathrm{d}t} = \boxed{\frac{k_1 k_2 K_\mathrm{a}^{1/2}}{k_1'} [\mathrm{HA}]^{3/2} [\mathrm{B}]}$

Q.5 The half-life period of a first-order decomposition of $N_2O_5(g)$ is expressed as

 $t_{1/2} = -30.3 + \frac{12581.78}{T}$ when time is expressed in sec. Find out (i) Frequency factor A, (ii) Energy of activation and (iii) fraction of the reactant undergoing the reaction in 1 hour at 300 K.

Sol.:

For a first order reaction,
$$ty_2 = \frac{0.693}{k_{obs}}$$

The reaction is
$$2N_2O_5 \rightarrow 4NO_2 + O_2$$

So, rate = $-\frac{1}{2} \frac{dEN_2O_5}{dt} = kEN_2O_5$
 $-\frac{dEN_2O_5}{dt} = 2kEN_2O_5$ = Kobs = $[N_2O_5]$

Here Kobs = 2K where K= rate constant

$$t_{V_2} = \frac{0.693}{Ae^{E/RT}} = \frac{0.693}{Ae^{E/RT}} = \frac{0.693}{Ae^{E/RT}}$$

Expressing t in secs and A in see and taking logarithm,

we have

$$\ln t_{V_2} = \ln \frac{0.693}{A} + \frac{E}{RT}$$

Compairing the equation with the given expression, we have

$$\int_{ln} \frac{0.693}{A} = -30.3$$
i.e. $A = 9.997 \times 10^{12}$ and $\frac{E}{R} = 12581.78$
i.e. $E = 12581.78 \times 1.987$ calmoi⁷ = 25 k calmet⁷
As time is expressed in sec, frequency factor = $9.997 \times 10^{12} \text{ sec}^{-1}$;
the unit is same on that of the rate constant.
So, rate constant,
 $K_{obs} = A e^{E/RT} = (9.997 \times 10^{12} \text{ sec}^{-1}) e^{-\frac{25070}{(1.987 \text{ outmet}^{1}/R^{-1})(300R)}}$
 $= 6.108 \times 10^{-6} \text{ sec}^{-1}$
 $t_{0} = \frac{1}{K_{obs}} \int_{ln} \frac{1}{1-0}$;
 $ln \frac{1}{1-0} = K_{obs} t_{0} = (6.108 \times 10^{-6} \text{ sec}^{-1}) \times (3600 \text{ sec})$
 $= 0.022$
 $\therefore 0 = 0.0217$
So, 0.0217 fraction of N20s decomposes at 27°C at the
end of 1 hr.

Q.6 For the mechanism

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$$A + B \xrightarrow{k_1} C ; C \xrightarrow{k_3} D$$

Derive the rate law using the steady state approximation to eliminate the concentration of C. Sol.:

Applying steady-state approximation,

$$\frac{d[C]}{dt} = k, [A] [B] - k_2 [C] - k_3 [C] = 0;$$

$$\therefore [C] = \frac{k_1 [A] [B]}{k_2 + k_3}$$

$$k_1 k_2 = \frac{k_1 [C] [C]}{k_2 + k_3}$$

Q.7 The enzyme-catalysed conversion of a substrate at 298 K has a Michaelis constant of 0.042 mol dm⁻³. The rate of the reaction is 2.45×10^{-4} mol dm⁻³ s⁻¹ when the substrate concentration is 0.890 mol dm⁻³. What is the maximum velocity of this enzymolysis?

Sol.:

The maximum velocity is k_b [E]₀ and the velocity in general is

$$v = k [E]_0 = \frac{k_b [S] [E]_0}{K_M + [S]} \text{ so } v_{\max} = k_b [E]_0 = \frac{K_M + [S]}{[S]} v$$
$$v_{\max} = \frac{(0.042 + 0.890) \text{ mol } \text{dm}^{-3}}{0.890 \text{ mol } \text{dm}^{-3}} (2.45 \times 10^{-4} \text{ mol } \text{dm}^{-3} \text{s}^{-1}) = \boxed{2.57 \times 10^{-4} \text{ mol } \text{dm}^{-3} \text{s}^{-1}}$$

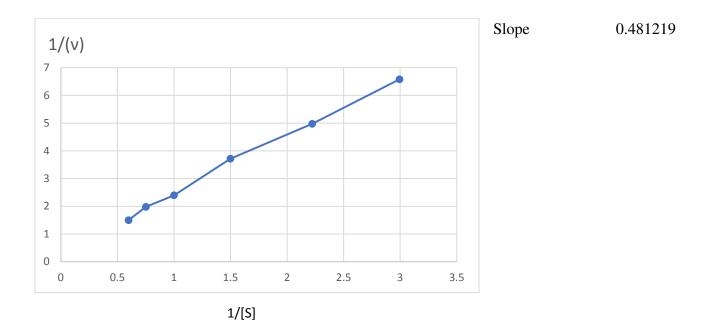
Q.8 The enzyme α -chymotrypsin is secreted in the pancreas of mammals and cleaves peptide bonds made between certain amino acids. Several solutions containing the small peptide Nglutaryl-l-phenylalanine-p-nitroanilide at different concentrations were prepared and the same small amount of α -chymotrypsin was added to each one. The following data were obtained on the initial rates of the formation of product:

| $[S]/(mmol dm^{-3})$ | 0.334 | 0.450 | 0.667 | 1.00 | 1.33 | 1.67 |
|---------------------------|-------|-------|-------|-------|-------|-------|
| $v/(mmol dm^{-3} s^{-1})$ | 0.152 | 0.201 | 0.269 | 0.417 | 0.505 | 0.667 |

Determine the maximum velocity and the Michaelis constant for the reaction.

Sol.: We draw up the following table:

| $[S]]/(mmol dm^{-3})$ | $(v)/(mmol dm^{-3} s^{-1})$ | 1/[S] | 1/(v) |
|------------------------|-----------------------------|----------|----------|
| 0.334 | 0.152 | 2.994012 | 6.578947 |
| 0.45 | 0.201 | 2.222222 | 4.975124 |
| 0.667 | 0.269 | 1.49925 | 3.717472 |
| 1 | 0.417 | 1 | 2.398082 |
| 1.33 | 0.505 | 0.75188 | 1.980198 |
| 1.67 | 0.667 | 0.598802 | 1.49925 |



Then we plot Lineweaver-Burk plot using the data. It should gives a straight line with a slope of $\frac{K_M}{v_{max}}$, a y-intercept at $\frac{1}{v_{max}}$ and x-intercept at $-\frac{1}{K_M}$. As we get negative intercept (-0.1673) at x-axis. So,

 $-\frac{1}{K_M} = -0.1673$

$$K_M = \frac{1}{0.1673} = 5.988 \text{ mmol dm}^{-3}$$

And

Slope = $\frac{K_M}{v_{max}} = 0.48$

$$\frac{5.988}{0.48} = v_{max}$$
$$v_{max} = 12.475 \text{ mmol dm}^{-3} \text{ s}^{-1}$$